

# FEASIBILITY STUDY OF ONCE THROUGH COOLING FOR 50 MW SOLAR THERMAL POWER PLANT ON/NEAR THE LOWER ORANGE RIVER

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# Introduction

## Background information

- With the technology advancement in CSP plants, the once -through cooling system has been neglected, due to a large amount of water passing through the condenser during operation.

# Introduction

## Background information

- In South Africa, 8 % of water is used in large industries and power generations, 18 % of water for rural and urban use, and 62 % of water resources are used for agriculture and irrigation (Roux *et al.*, 2012).

# Introduction

## Problem statement

- Agriculture and irrigation sector in South Africa consume more water resources than other sector.
- Low thermal efficiency in CSP plant using air - cooled system

# Introduction

## Aims and objectives

- To analyze the possibility of diverting water that passed through a condenser to agricultural purposes or not.
- To compare the improved thermal efficiency against condenser fouling factor.

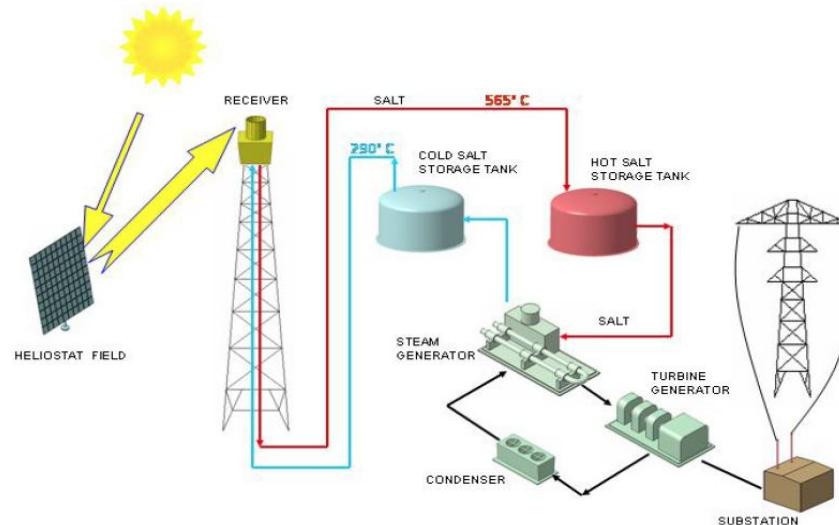
# Introduction

## Aims and objectives

- To compare the improved thermal efficiency against air - cooled efficiency.
- To identify the agricultural constraints.

# CSP Plant

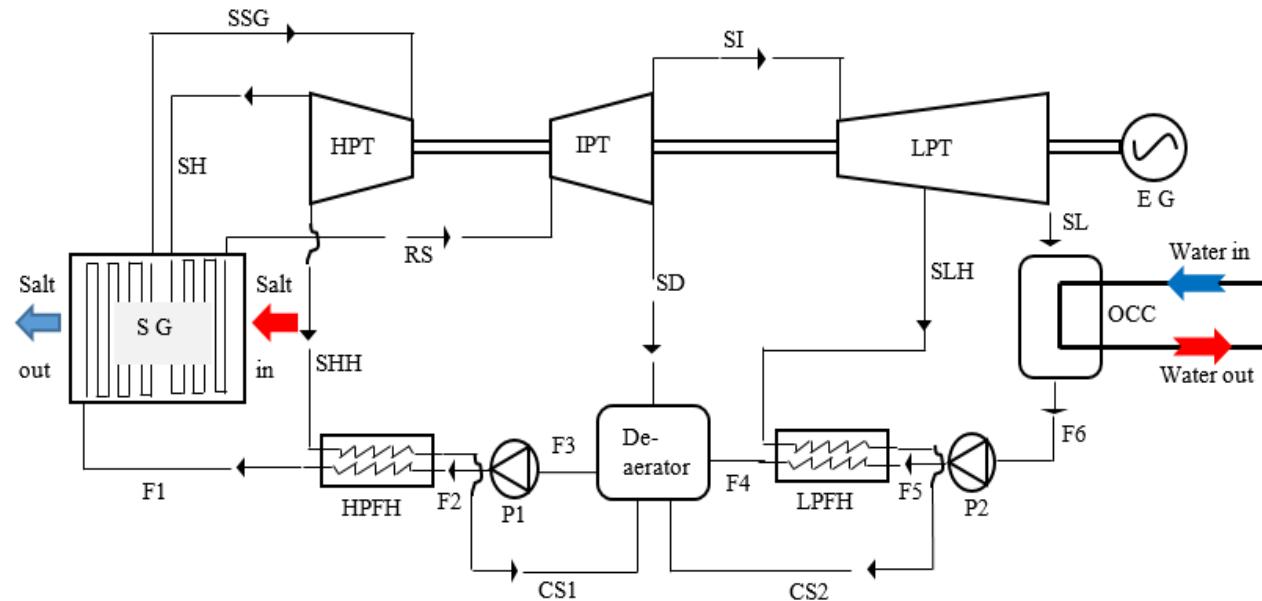
## Modelling



# CSP Plant



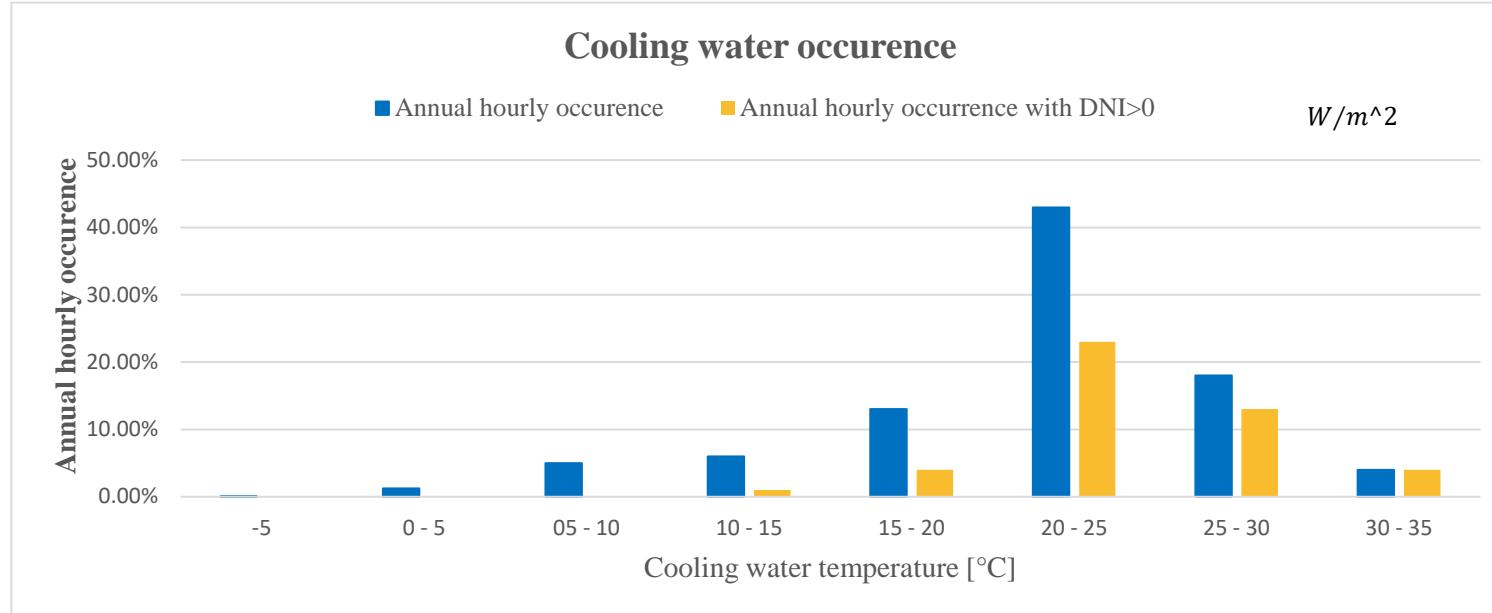
# Modelling



# CSP Plant



## Orange river temperature



# CSP Plant

## Modelling assumptions

- Steam pressure at outlet steam generator = 130 MPa
- Steam temperature at outlet steam generator = 540 °C
- Reheat temperature = 540 °C
- Electric Generator efficiency = 0.98
- Inlet cooling water temperature = 21.1 °C

# CSP Plant

## Modelling assumptions

- Feed - water heater at inlet steam generator = 130 MPa
- Feed - water heater temperature at inlet steam generator = 220 °C
- Temperature rise across each feed - water heater are equal

# CSP Plant

## Modelling assumptions

- Total power output at the electric generator = 50 MW<sub>e</sub>
- Exit pressure pump (P2) is equal to the Deaerator pressure
- Exit pressure pump (P2) is equal to the inlet pressure at the steam generator

# CSP Plant

## Modelling assumptions

- The efficiency of high pressure turbine = 0.90
- The efficiency of intermediate pressure turbine = 0.85
- The efficiency of low pressure turbine = 0.82

# CSP Plant

## Modelling

- Steam generator

$$\dot{Q}_{SG} = \dot{m}_{F1}(h_{SSG} - h_{F1}) \quad \dot{Q}_{RH} = \dot{m}_{SSG}(h_{RS} - h_{SH})$$

$$\dot{m}_s \bar{C}_{ps}(T_{is} - T_{os}) = \dot{m}_{F1}(h_{SSG} - h_{F1}) + \dot{m}_{SH}(h_{RS} - h_{SH})$$

- Turbine

$$w_{HPT} = \dot{m}_{SH}(h_{SSG} - h_{SH}) + \dot{m}_{SHH}(h_{SSG} - h_{SHH})$$

$$w_{IPT} = \dot{m}_{SI}(h_{RS} - h_{SI}) + \dot{m}_{SD}(h_{RS} - h_{SD})$$

$$w_{LPT} = \dot{m}_{SL}(h_{SI} - h_{SL}) + \dot{m}_{SLH}(h_{SI} - h_{SLH})$$

- Feed pump

$$w_{P1} = \dot{m}_{F3}(h_{F2} - h_{F3})$$

$$w_{P2} = \dot{m}_{F6}(h_{F5} - h_{F6})$$

# CSP Plant

## Modelling

- Feed - water heater

$$T_r = \frac{T_{F1} - T_{F5}}{N_{fwh}} \quad \dot{m}_{SHH} (h_{SHH} - h_{CS1}) = \dot{m}_{F2} (h_{F1} - h_{F2})$$

$$\dot{m}_{F3} (h_{F3}) = \dot{m}_{F4} (h_{F5}) + \dot{m}_{CS1} (h_{CS1}) + \dot{m}_{CS2} (h_{CS2}) + \dot{m}_{SD} (h_{SD})$$

$$\dot{m}_{SLH} (h_{SLH} - h_{CS2}) = \dot{m}_{F5} (h_{F4} - h_{F5})$$

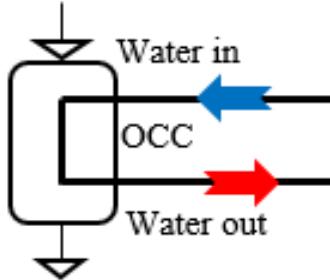
- Thermal efficiency

$$W_{net} = w_T - w_{TP} \quad \eta_t = \frac{W_{net}}{\mathbb{Q}_T}$$

# CSP Plant



## Condenser modelling



$$T_{cwo} = \frac{Q_{max}}{\dot{m}_{cw} c_{p,cw}} + T_{cwi}$$

$$\Delta T_{C,w} = T_{cwo} - T_{cwi}$$

$$TTD = T_s - T_{cwo}$$

$ITD = T_s - T_{cwi}$  Cooling water output temperature = 28.1 °C

Change in cooling water temperature = 7 °C

Terminal temperature difference = 5 °C

$$R''_{fc} = \pi d_1 L_{eff} \left[ \frac{\left( T_{C,si} - T_{C,wo} \right) - \left( T_{C,so} - T_{C,wi} \right)}{Q_{c,m} \ln \left( \frac{T_{C,si} - T_{C,wo}}{T_{C,so} - T_{C,wi}} \right)} - \left( \frac{\pi d_2 L_{eff} k_{fs}}{d_3 - d_2} N u_s \right)^{-1} - \frac{\ln \left( \frac{d_2}{d_1} \right)}{2 \pi k_t L_{eff}} - \left( \pi L_{eff} k_{fw} \frac{\left( \frac{f_D}{8} R e_w P r_w \right)}{1 + 12.7 \left( \frac{f_D}{8} \right)^{0.5} (P r^{2/3} - 1)} \right)^{-1} \right]$$

# CSP Plant

## Results

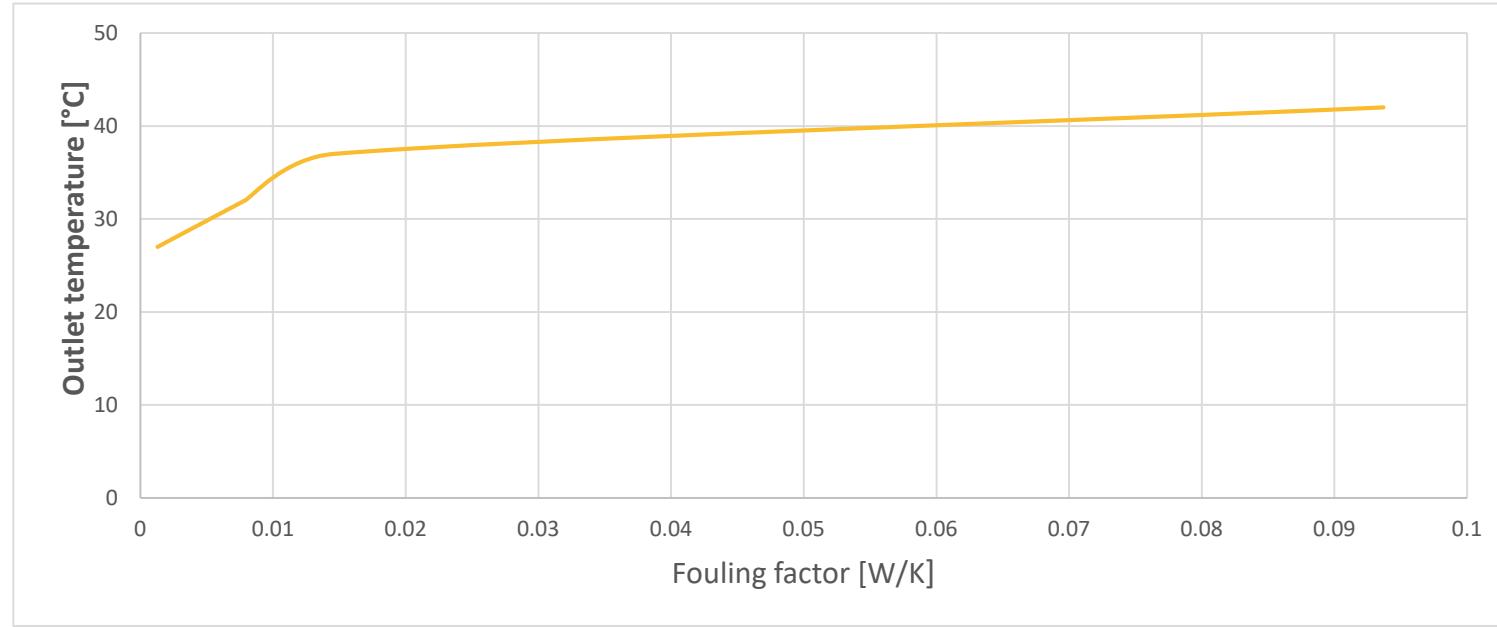
	Units	Once-through cooling	Air-cooled
Energy supplied to steam generator	kJ/kg	104719.3	111555.2
Efficiency	%	47.7	44.8
Mass flow rate	kg/s	35.54	37.86
Power output	MW <sub>e</sub>	50	50

	Units	Once-through cooling	Air-cooled
Energy supplied to steam generator	kJ/kg	104719.3	104719.3
Efficiency	%	47.7	44.8
Mass flow rate	kg/s	38.98	38.98
Power output	MW <sub>e</sub>	50	47

# CSP Plant



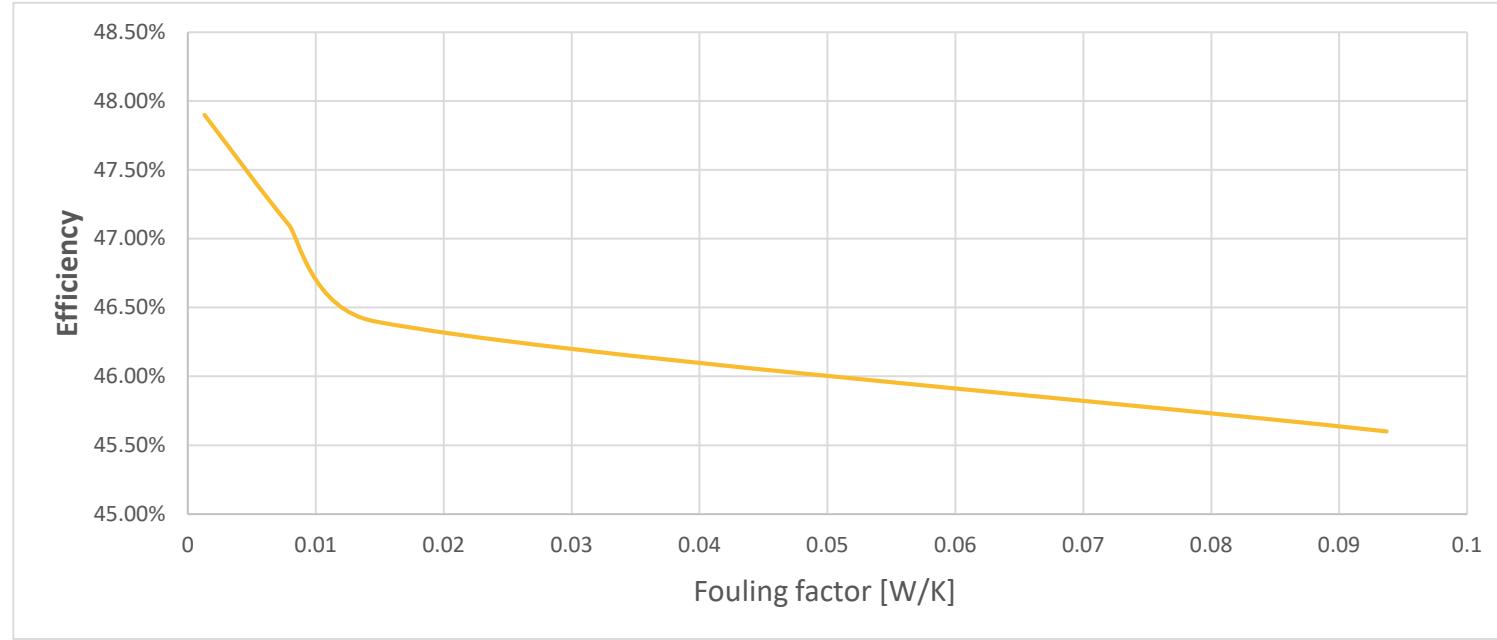
## Results



# CSP Plant



## Results



# CSP Plant

## Results

- Agricultural constraint includes government policy, water demand and water temperature

# CSP Plant



## Conclusion

- Once through cooling could be used to increase the CSP plant performance and at the same use the discharge water for agricultural purposes.

# THANK YOU

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## ACKNOWLEDGEMENTS:

Dr. J. Hoffmann.

# Questions?

## CONTACT DETAILS:

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