



#### The Feasibility of Solar Thermal Process Heat for the Sugarcane Industry in South Africa

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3<sup>rd</sup> Annual STERC SolarPACES Symposium 14 & 15 July 2015 Stellenbosch, South Africa





### Agenda

#### **Overview**

- Overview of the S.A. Sugar Industry
- Raw Sugar Production
- Drivers of Innovation
- SPH Technology & Low Hanging Fruit
- Potential of SPH Integration
- Expected Results

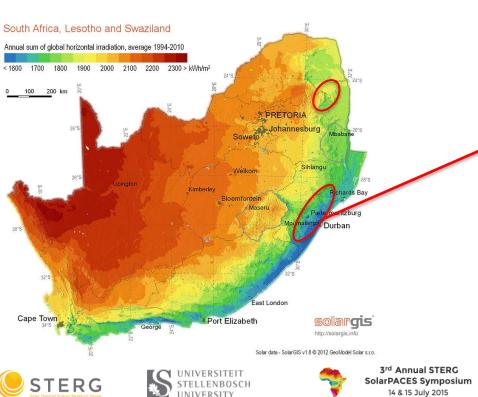








#### Location



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#### **Overview**

Location:	KZN & Mpumalanga	
Production:	> 2m tons/a	(20m tons cane)
Season:	March - December	
Contribution:	R12b per year	
Employment:	79 000   12 750	
Sugar Milling:	14 Raw Sugar Factories	
Market:	Highly Regulated Prices	
SMRI:	Profitability, Efficiency & Innovation	

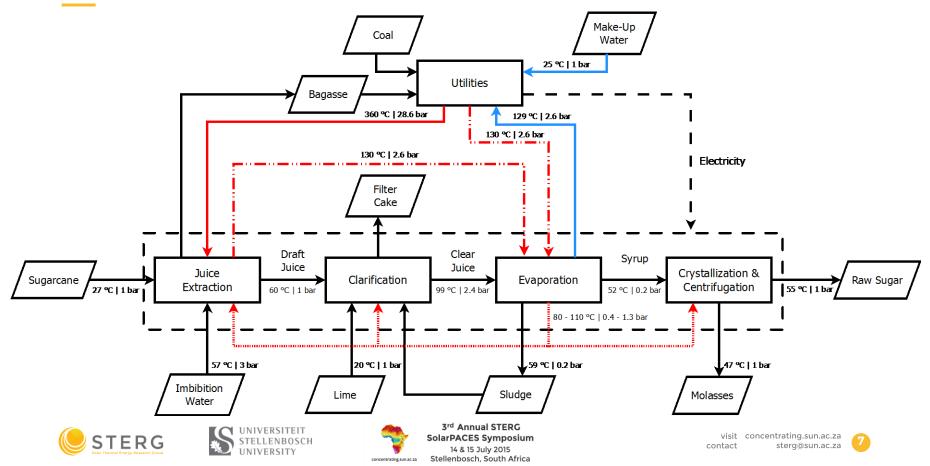








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### **Drivers of Innovation**

Economic Pressure: Low Prices, Rising Input & Operational Costs

- $\rightarrow$  Reduce Operational Costs
  - Reduce Coal Consumption
- $\rightarrow$  Explore Alternative Income Streams
  - Bagasse By-Products
  - Bio-Ethanol
  - Electricity Cogeneration







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#### **Technology Characteristics**

Temperatures: Pressure: Integration: Power and gain: Potential Gain: System size: 25 - 450 °C Up to 40 bar Supply Level / Process Level 700 W<sub>p</sub>/m<sup>2</sup> peak power Up to 1 MWh/m<sup>2</sup> per annum No technical limit (Area, Capital)



**Fresnel Collector** 



Parabolic Trough Collector



Central Tower Receiver



**Flat-Plate Collectors** 



**Evacuated Tube Collectors** 



Stationary Concentrating Collector







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#### Potential for the Sugar Industry

- Objective:Identify & Assess Suitable SPH Integration PointsMethodology:1. Develop a flow diagram of a generic sugar mill
  - 2. Analyse the energy consumption
  - 3. Identify potential SPH integration points
  - 4. Assess & rank the integration points
  - 5. Develop concept designs
  - 6. Estimate the potential solar gains
  - 7. Assess the techno-economic feasibility





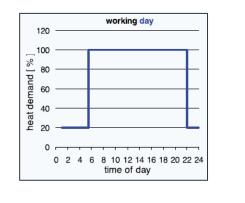


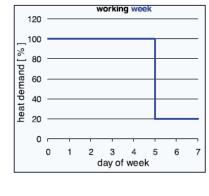


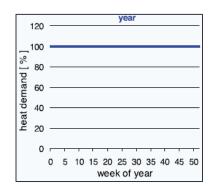
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#### **Low Hanging Fruits**

- Low Process (Return) Temperature
- High Temperature Lift
- High & Constant Heat Demand
- Demand Concurs with High Irradiance











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#### **Solar Process Heat Integration** $\langle \rangle$ Let-Down Make-Up Valve Coal Water Live Exhaust Steam Steam **Turbo-Alternators** Boiler 360 °C 130 °C 28.6 bar 2.6 bar Prime Movers Evaporator 1 Cane Condensate . . . . . . . . . . . . . . . . . . . Raw **Boiling House** Clarification Drying Diffuser ₽ **Evaporator 2** Sugar Bagasse Vapour 1 Vapour 2 Vapour 3 Evaporator 3 120 °C 110 ℃ 95 °C 2 bar 1.4 bar 0.8 bar Evaporator 4 3<sup>rd</sup> Annual STERG STERG visit concentrating.sun.ac.za SolarPACES Symposium sterg@sun.ac.za contact

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### **Entry Barriers**

- Low Cost of Energy:
- Heat Distribution:
- Seasonality:
- Relatively Low Irradiation:
- Area Requirements:

Bagasse Exhaust, Vapour March – December 2000 kWh/m² Limited Area









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#### **Potential Integration Points**

Heat Sink	Fuel / Heat Source	Process Temperature	Temperature Lift	Mean Load
Live Steam Injection	Bagasse & Coal	360 °C	N/A	90 MW
Feed Water Pre-Heating	Bagasse & Coal	129 °C	230 °C	75 MW
Make-Up Water Pre-Heating	Bagasse & Coal	25 °C	335 °C	N/A
Evaporation	Exhaust Steam	114 °C	7 °C	58 MW
Clear Juice HEX	Exhaust Steam	100 °C	14 °C	4 MW
Sugar Drying	Exhaust Steam	25 °C	55 °C	0,6 MW
Bagasse Drying	Bagasse & Coal	72 °C	N/A	N/A
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### **Thank You**

#### **ACKNOWLEDGEMENTS:**

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